



Bio-CCS in power and CHP production with high biomass shares

Workshop: Biomass with CCS - Removing CO₂ from the Atmosphere, 19.6.2012, Brussels

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Biomass combustion in power and CHP plants

Different co-firing technologies in PC

- direct co-firing (mixing of biomass with coal or separate biomass feeding)
- indirect co-firing (gasification, pyrolysis, separate biomass boiler with integrated steam cycle)
- biomass shares relatively small (especially in direct co-firing)

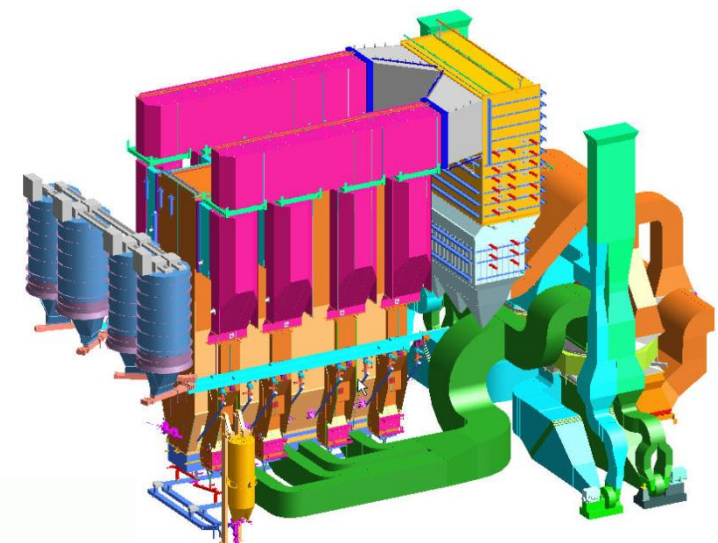
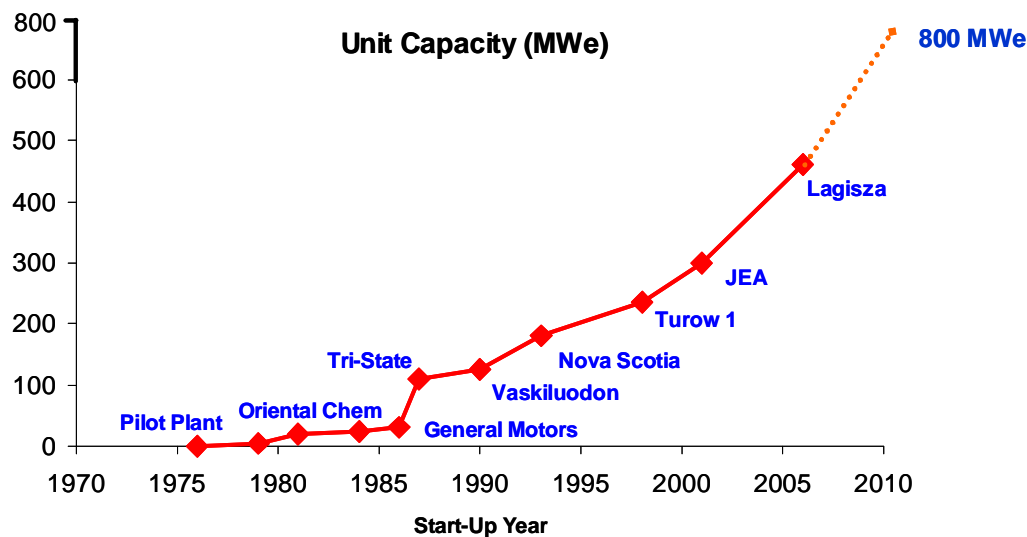
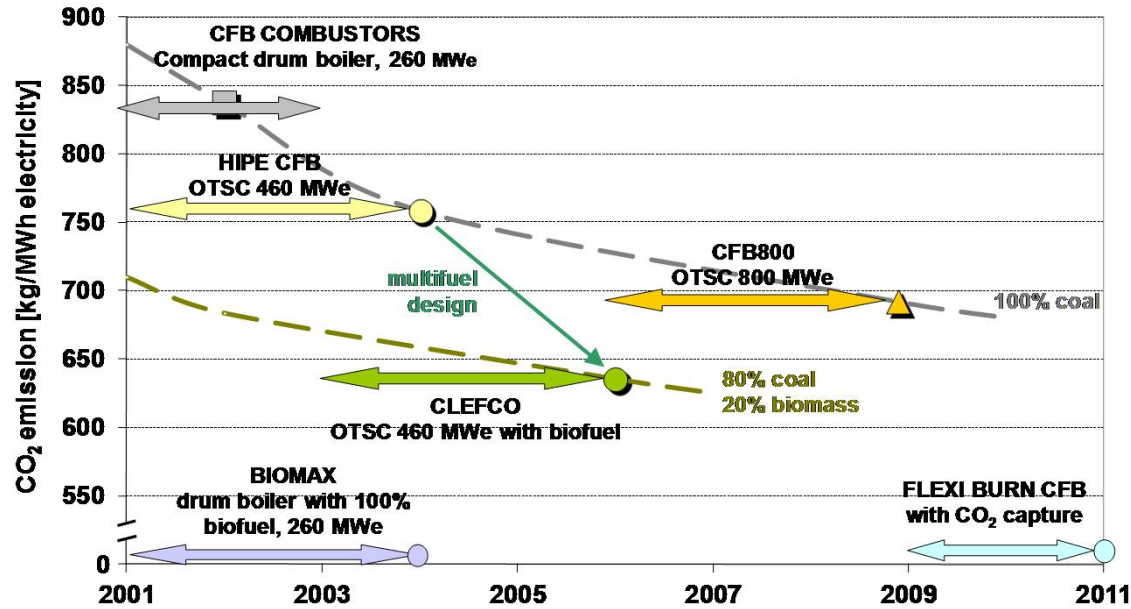
Dedicated/high-share biomass plants

- grate combustion in small scale
- **fluidised bed combustion** has become the dominant technology in larger plants
- typical size of dedicated biomass power and CHP plants is smaller than PF coal plants (mainly due to fuel availability)



Development of CFB technology under EU programs

FP5: CFB Combustor, HIPE CFB, BIOMAX
RFCS: CLEFCO, CFB800
FP7: FLEXI BURN CFB, O2GEN



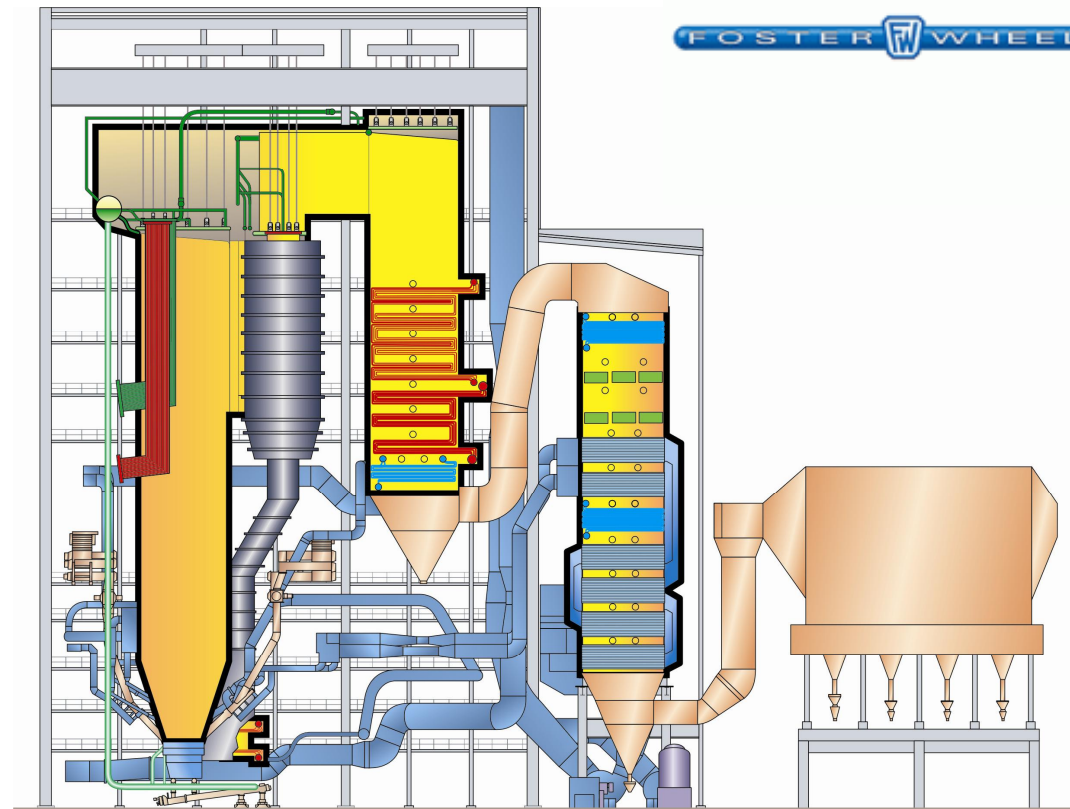
The World's largest 100% biomass CFB

GDF Suez Energia Polska S.A.
Połaniec
Poland

Steam 447 MW_{th}
153/135 kg/s
128/20 bar
535/535 °C

Fuels
Wood 0 – 100 %
Agro 0 – 20 %
straw, sunflower pellets,
dried fruit (marc), and
palm kernel

Start-up 2012



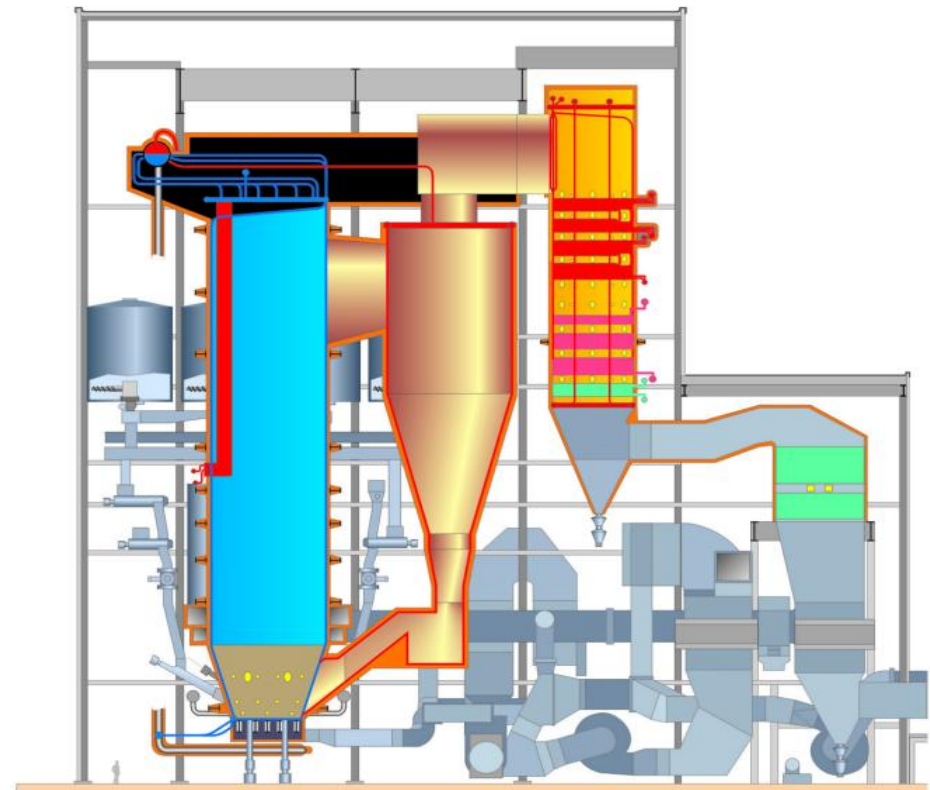
Possibility to utilise **100% biomass** in co-fired CFB

Alholmens Kraft,
Pietarsaari, Finland



CFB technology:

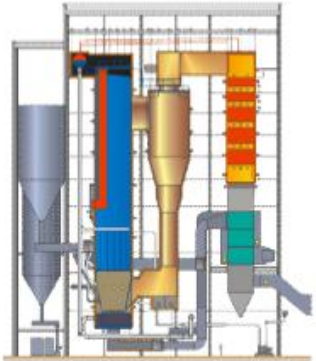
- 550MW_{th}
- 194kg/s , 165bar , 545°C
- Uses 40 % peat, 20 % coal, 30 % of biomass (forest residues, industrial wood and bark etc.) and 10 % SRF.
- The design of the plant allows great fuel flexibility, the boiler is able to combust all mixtures from **100 % biomass** to 100 % coal.



Towards negative CO₂ emissions with CFB technology

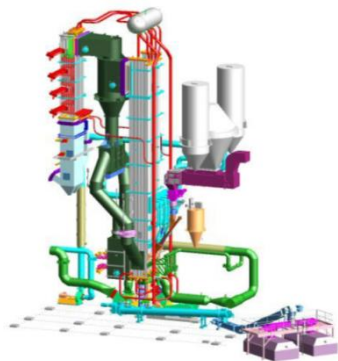
Fossil

- Low solids
- High solids



- High plant efficiency
- Fossil CO₂ emissions

Fossil with CO₂ capture

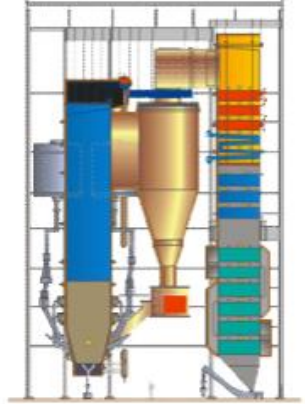


- 5...10 %-pts eff. penalty in CCS
- Up to 95% CO₂ capture rates

Higher OPEX and CAPEX than without capture

Bio/Multi

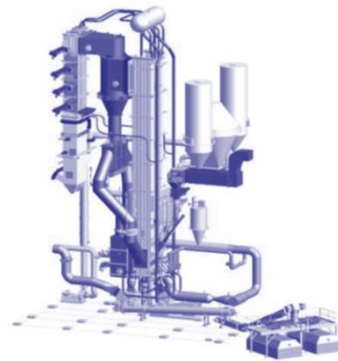
- Agro
- Wood



- Good plant efficiency
- Zero (biogenic) CO₂ emissions

Higher OPEX and CAPEX than with fossil fuels

Bio/Multi with CO₂ capture

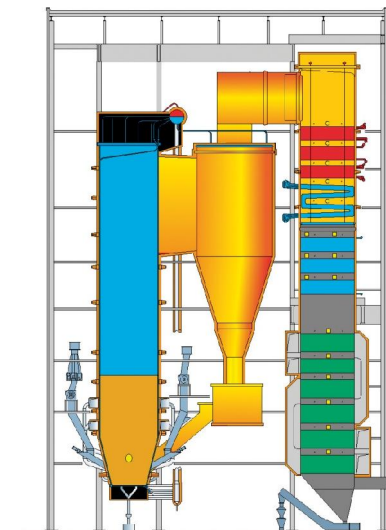
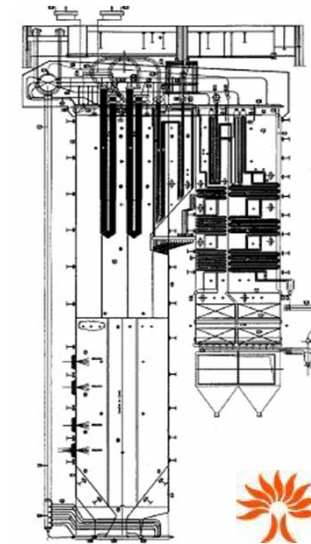


- Efficiency penalty similar to fossil
- "Negative" CO₂ emissions

Highest OPEX and CAPEX

The advantages of CFB technology compared to PC in oxy-combustion

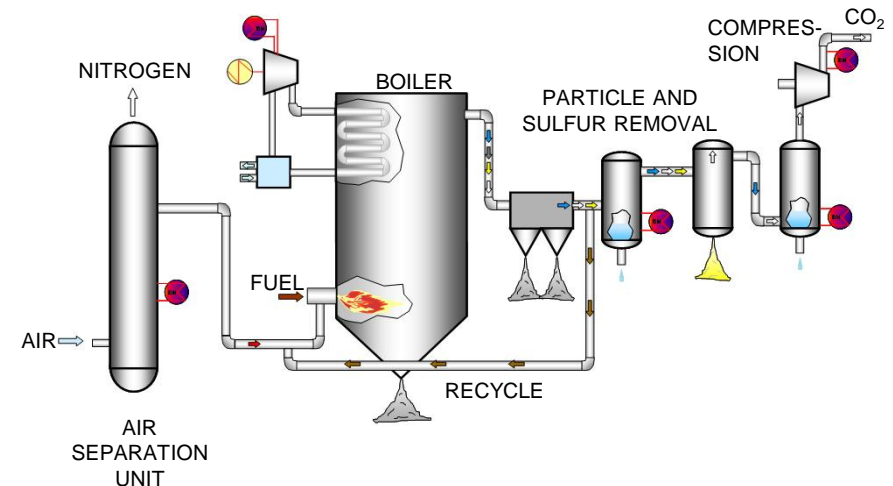
- Competition between PC and CFB in oxygen-firing is somewhat similar to the air-firing case, with differences in fuel and process flexibility, emissions with or without flue gas cleaning equipment ash streams, etc.
- The **flexibility of CFB under varying load conditions** offers benefits in retaining more uniform furnace temperature profiles (in air-firing as well as oxygen-firing).
 - **Lower NO_x emissions** compared to PC
 - Enables more extensive process optimisation possibilities with **higher O₂ concentrations** which results in smaller furnace size and therefore improves economy of oxy-CFB vs. oxy-PC.
- Limestone addition into the furnace for sulphur capture can **ease separation of CO₂ from flue gas**. In the case of large biomass shares, the additional SO_x removal investment is not needed.
- CCS always reduces the overall power plant efficiency, irrespective of the technology. However, high fuel flexibility offers an additional benefit for CFB technology to **compensate the costs of CCS by applying low-quality fuels**.



CO₂ capture options for biomass (co-)fired boilers (CFB/PC)

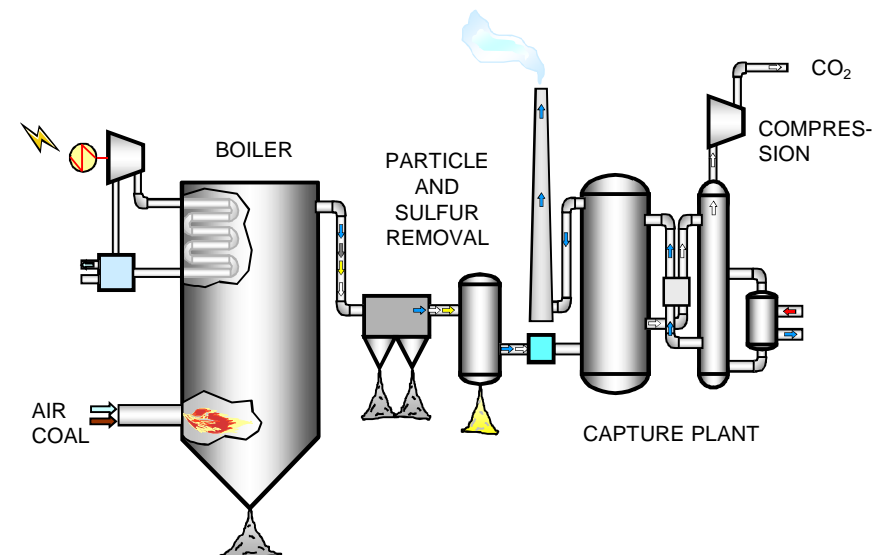
Oxyfuel combustion

- More suitable for greenfield plants (challenges with air ingress in retrofit)
- Main energy penalty due to ASU electricity consumption
- Flexiburn concept for air or oxy-fired operation modes (in CFB)
- Possible challenges with boiler design due to flue gas properties (e.g. enrichment of impurities)



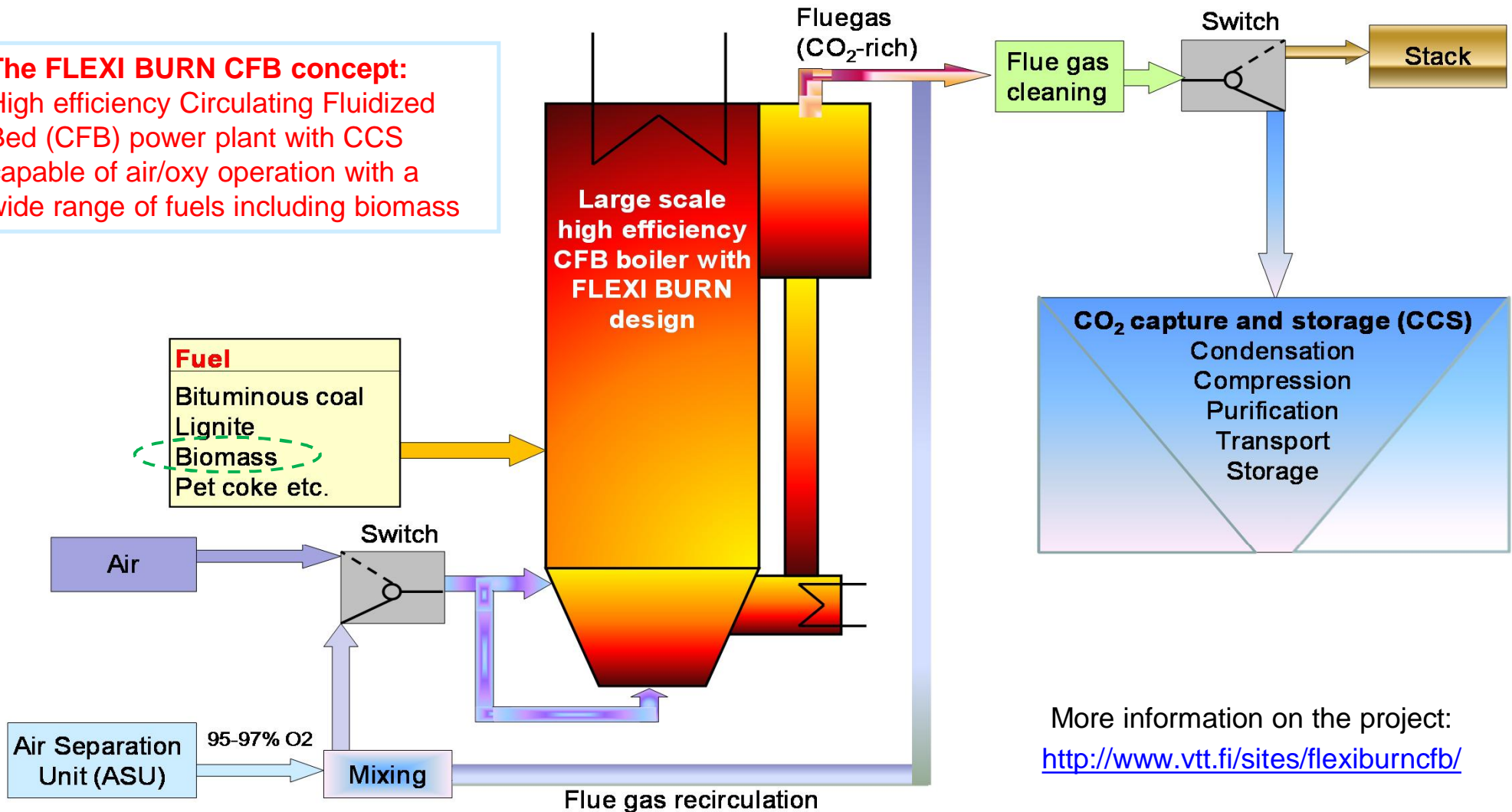
Post combustion

- Suitable also for retrofit (challenges with on-site space requirements)
- Main energy penalty due to steam need for solvent regeneration
- Possibility to by-pass the capture plant during profitable market conditions
- Possible challenges with solvent related emissions (e.g. nitrous amines) and waste disposal



FLEXI BURN CFB allowing operation under normal air-firing as well as oxygen-firing with CCS

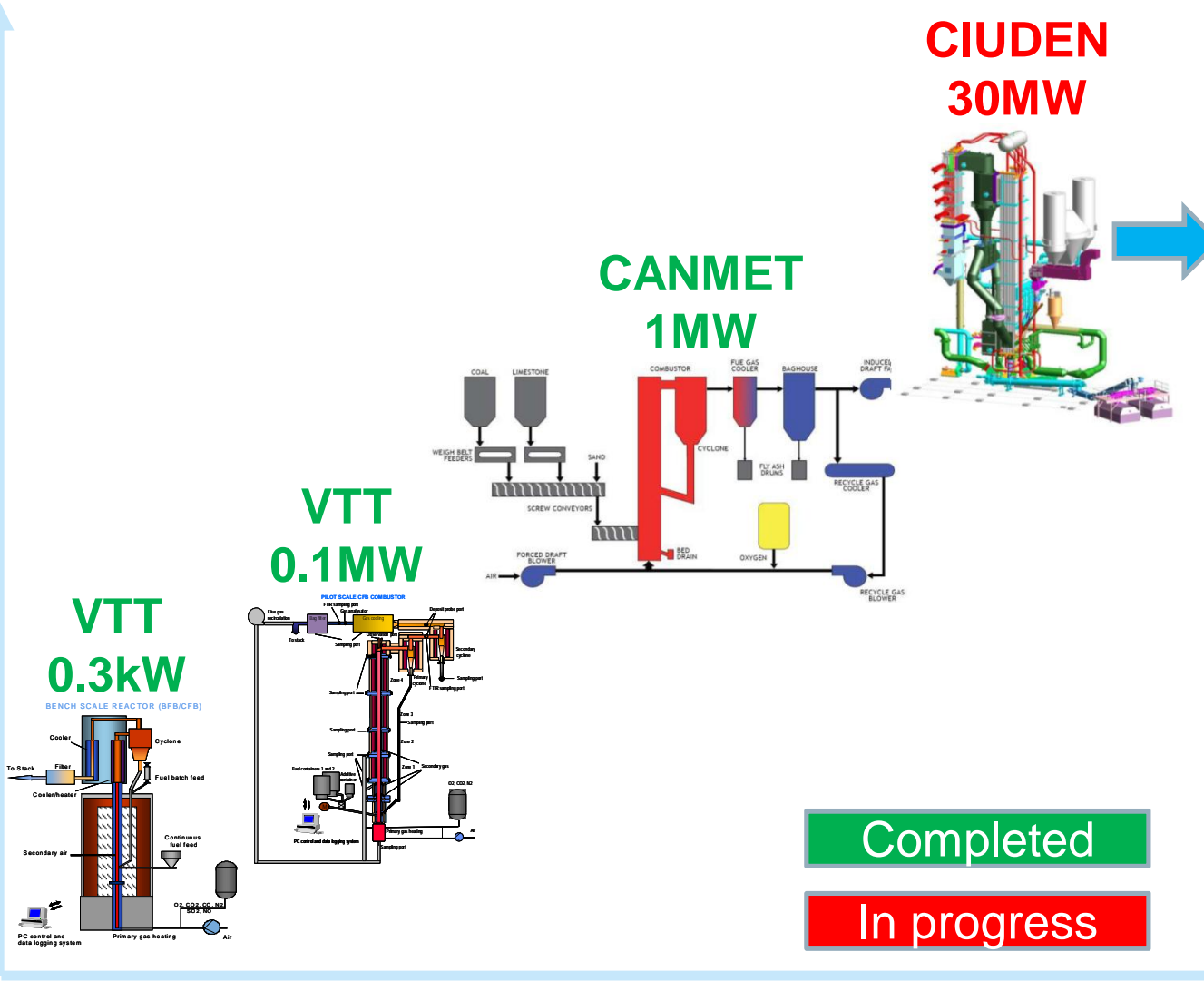
The FLEXI BURN CFB concept:
 High efficiency Circulating Fluidized Bed (CFB) power plant with CCS capable of air/oxy operation with a wide range of fuels including biomass



More information on the project:
<http://www.vtt.fi/sites/flexiburncfb/>

FLEXI BURN CFB – Demonstration steps

Demonstration scales



Concept for 300 MW_e



Aim: to develop and demonstrate FLEXI BURN CFB concept enabling to reach the target of near zero emission power plants

Post-2020 target:
Full 800 MW_{e, gross} commercial plant

Completed
In progress

2009

Time

2012

OXY-CFB-300 Compostilla Project CCS Value Chain



CAPTURE TECHNOLOGY

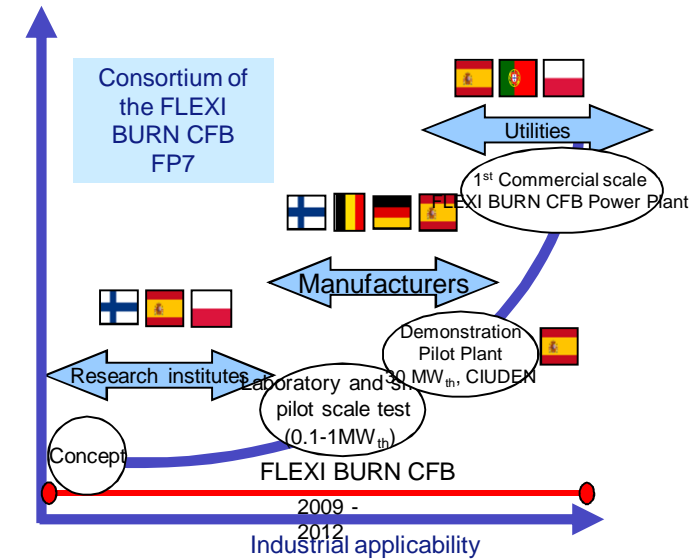
- OXY-CFB supercritical boiler; wide design fuel range (domestic and imported), including **biomass**.

CO₂ TRANSPORT

- 12" / 16" underground pipeline; 135 km.
- 5,500 ton/day; ~ 120 bar

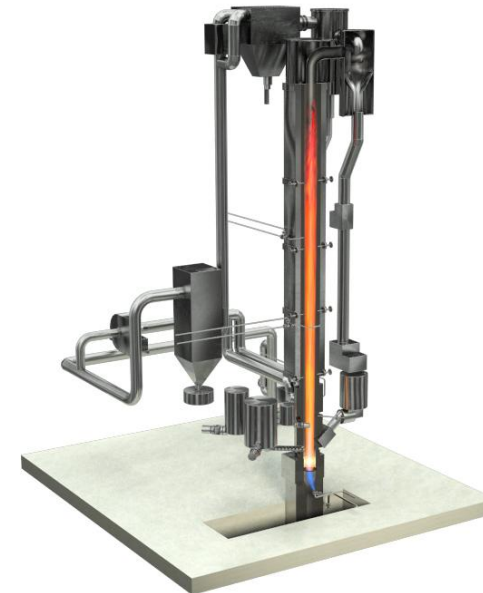
CO₂ STORAGE

- Deep saline formation
- Duero basin (optional: Ebro basin)



Flexiburn: Pilot scale CFB experiments (0.1MW) under air- and oxygen-firing conditions

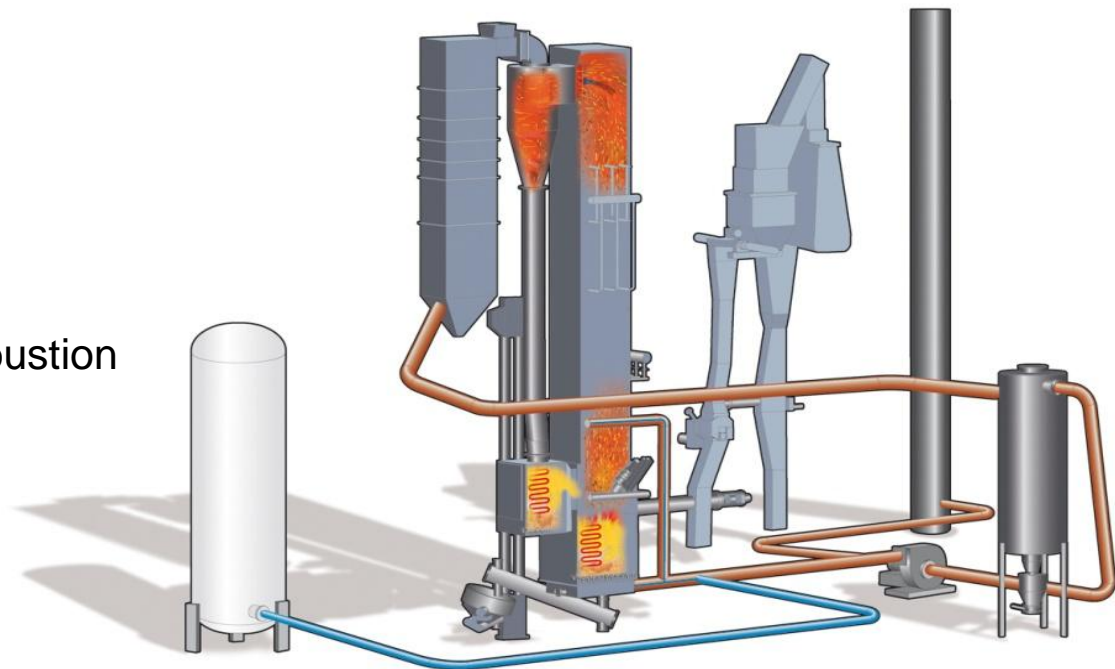
- Combustion tests have been carried out with pilot scale and bench scale test rigs at VTT in Finland
- Tests provide a base for development and validation of the design tools needed in the concept development
- Also some **biomass fuels** have been tested (straw pellet and good quality wood chips)



Fuels	Mixture ratio on energy basis (LHV wet)	Mixture ratio on mass basis (wet)
Anthracite + Pet-coke	55/45	70/30
Anthracite	100	100
Bituminous coal (Polish)	100	100
Lignite (Spanish) + South African coal	55/45	70/30
Anthracite + wood	90/10	85/15
Bituminous coal (Polish) + straw pellet	80/20	75/25

Successful CFB Oxy-combustion Pilot Project

- Oxy-combustion CFB boiler
 - Location in Metso test plant in Tampere
 - *Preliminary tests at VTT*
- Project participants
 - Metso and Fortum
- Target
 - To scale up CFB oxyfuel combustion from laboratory to pilot scale
- Test figures
 - Size 4MW_{th}
 - 5 weeks test runs in 2010
 - Two fuels tested



Feasibility of Bio-CCS in CHP production

- *Case Study of Biomass Co-firing Plant in Finland*



Conceptual CCS case studies by VTT (conducted & upcoming)

	Power plant	CHP-plant	Steel mill	CHP-plant	CHP-plant	Steel mill	CHP-plant	CLC-plant
Location	western Finland	central Finland	northern Finland	western Finland	southern Finland	northern Finland	northern Finland	western Finland
Fuel power	1300 MW	500 MW	-	482 MW	919 MW	-	300 MW	482 MW
Capture potential	3 Mt/a	1.5 Mt/a	2.5 Mt/a	1.4 Mt/a	1.3 Mt/a	2.5 Mt/a	1 Mt/a	?
Combustion tech.	PF	CFB	-	CFB	GTCC	-	CFB	CFB
CCS tech.	PCC	oxy/PCC	PCC	oxy	PCC	OBF	PCC	oxy (CLC)
Fuel	coal	peat	process gas	cofiring/ biomass/peat	natural gas	process gas	peat/biomass	?
Type	retrofit	greenfield	retrofit/ rebuilt	greenfield	retrofit	retrofit/ rebuilt	retrofit	greenfield

- Based on real industrial plants and environments
- Modeling of the plants with and without CCS applied
- Techno-economic evaluation of the overall feasibility (including transportation and storage)
- Costs and emission reduction from the investor's point of view



Economic trade-off for CO₂ capture plant investor



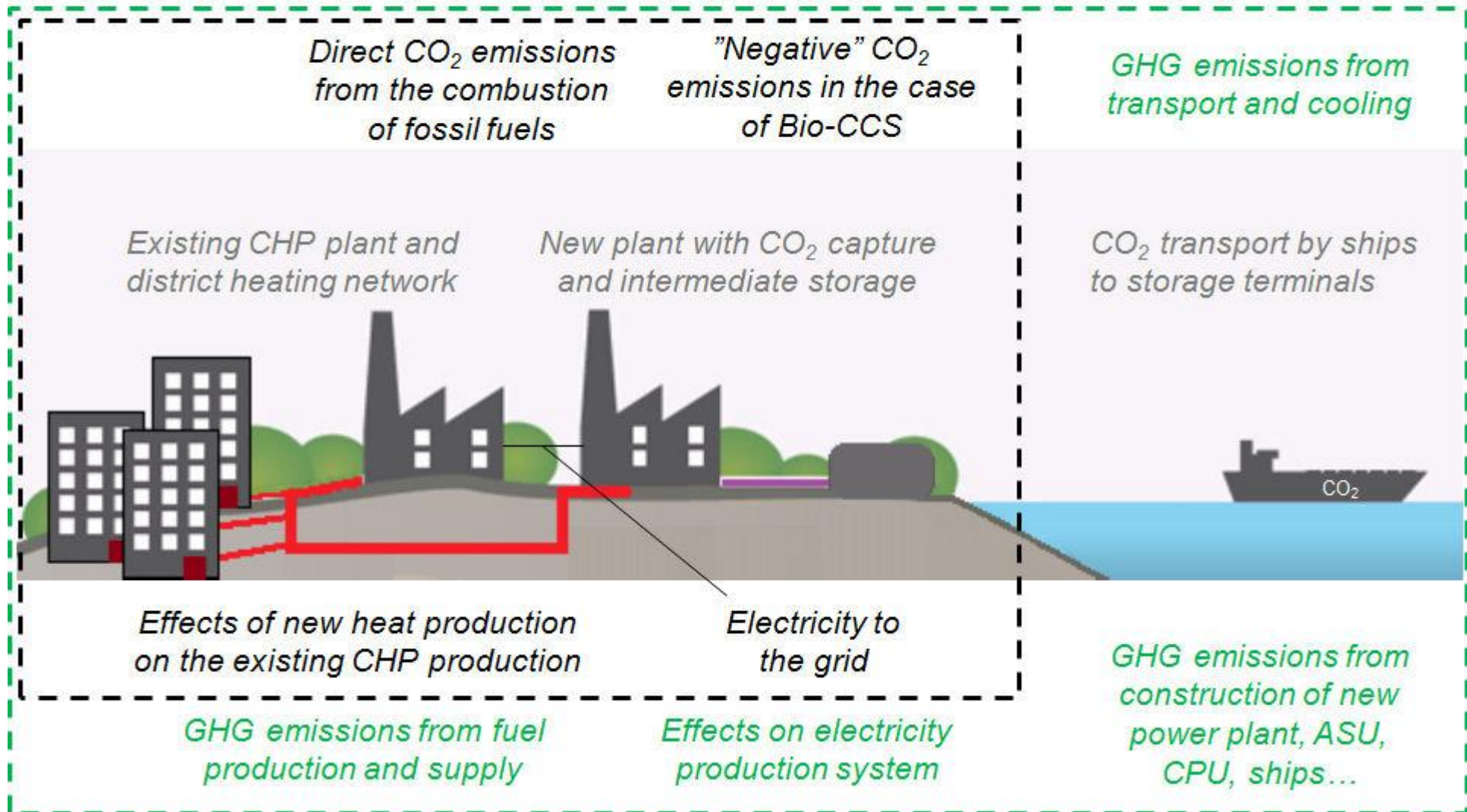
- Feasibility of CCS is very sensitive for CO₂ allowance and electricity prices
 - Interaction between CO₂ allowance and electricity price
 - Sensitivities also for fuel prices, efficiencies, investments etc. need to be clarified
- System model CC-Skynet™ has been developed at VTT to evaluate the most critical questions with focus on the impacts on the case specific plant and the **surrounding energy system**

Case study introduction

- The case study for economic and environmental implications of Bio-CCS is based on greenfield 482 MW_{fuel} CHP-plant situated on the coast of the Gulf of Bothnia and emitting approximately 1.5 Mton CO₂ / year. The plant is equipped with a modern **CFB-boiler** which is using **oxy-fuel technology** in the CCS applications.
- The economics of CCS were evaluated from investor's (local energy company) point of view including the effects on existing energy system
- In the study it is assumed that **the economic incentive for negative CO₂ emission is included in EU ETS.**
- In the studied system **existing CHP-plant** and the new plant produce district heat and back-pressure electricity with given utilization rates and condensing electricity is produced **at the new plant** depending on the given utilization rates.

Studied system and selected boundaries

- - · GHG emissions considered in BEP's (system boundary from the operator's point of view)
- - - · GHG emissions considered in LCA (system boundary from the global point of view)



The studied cases are named as follows

1. **Reference:** No new plant. The existing CHP-plant produces district heat and back-pressure electricity with maximum load (utilization rate 6000 h/a) and number of heavy-oil fired district heating plants provide the additional heat needed within the system.

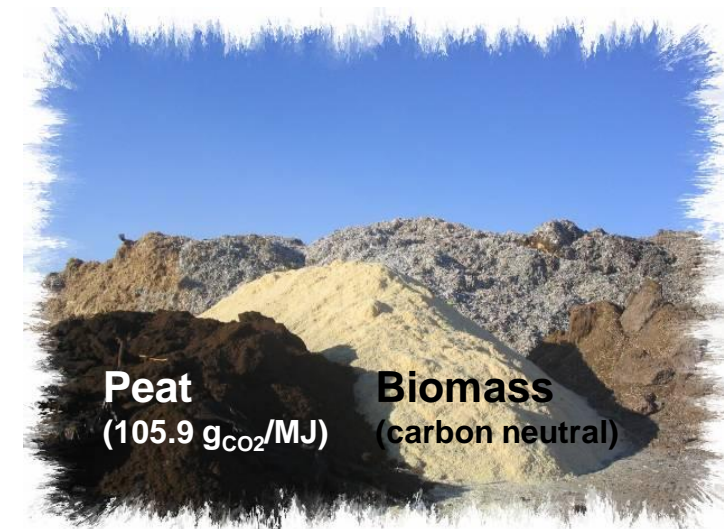
2. **peat w/o CCS**
3. **peat with CCS** } The new plant is fired with 100 % peat

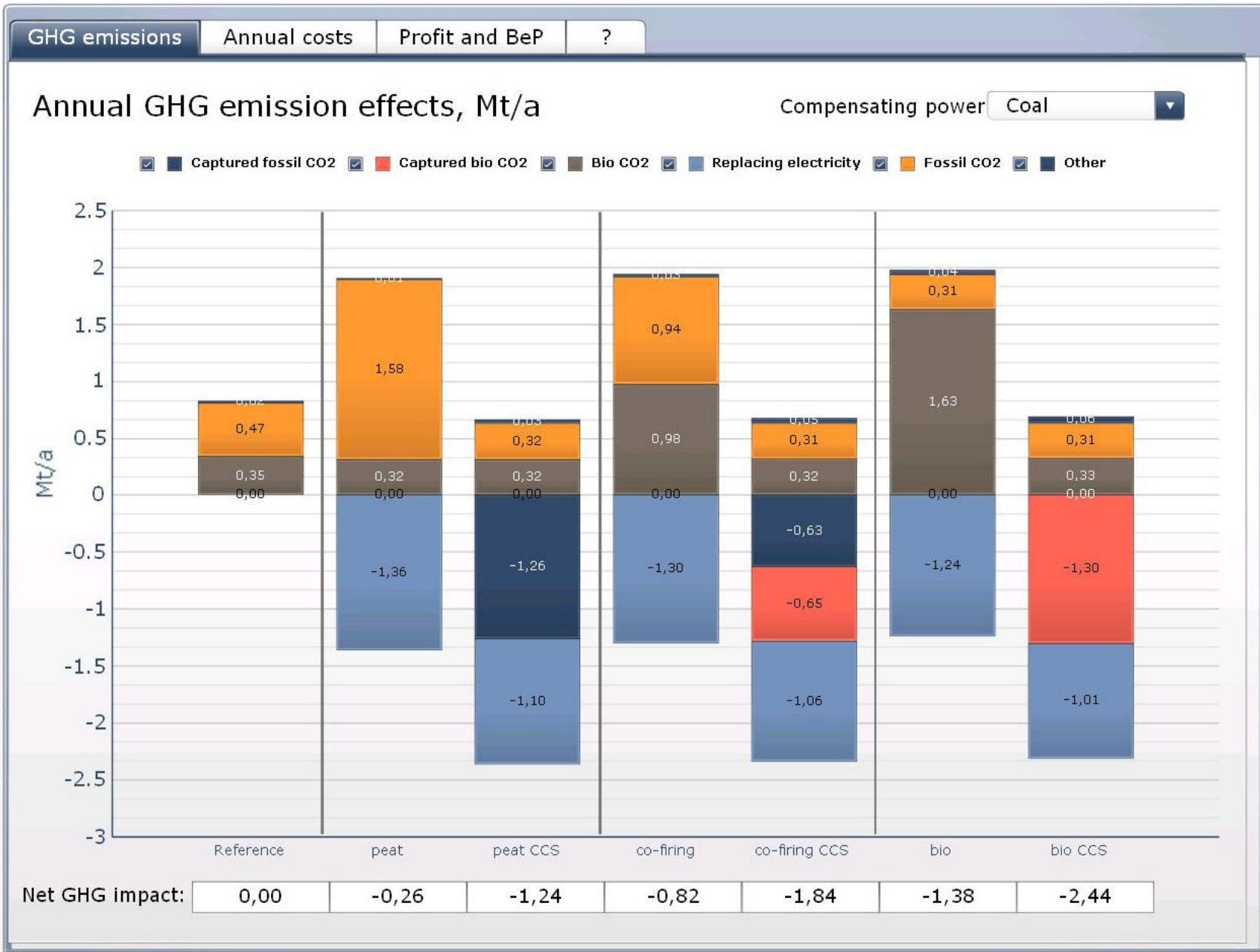
4. **co-firing w/o CCS**
5. **co-firing with CCS** } The new plant is fired with 50 % peat and 50 % biomass

6. **bio w/o CCS**
7. **bio with CCS** } The new plant is fired with 100 % peat

In every case the existing CHP-plant is fired with 50 % peat and 50 % biomass.

Biomass prices are case-specific due to (possible) price increase with higher volumes





GHG emissions

Annual costs

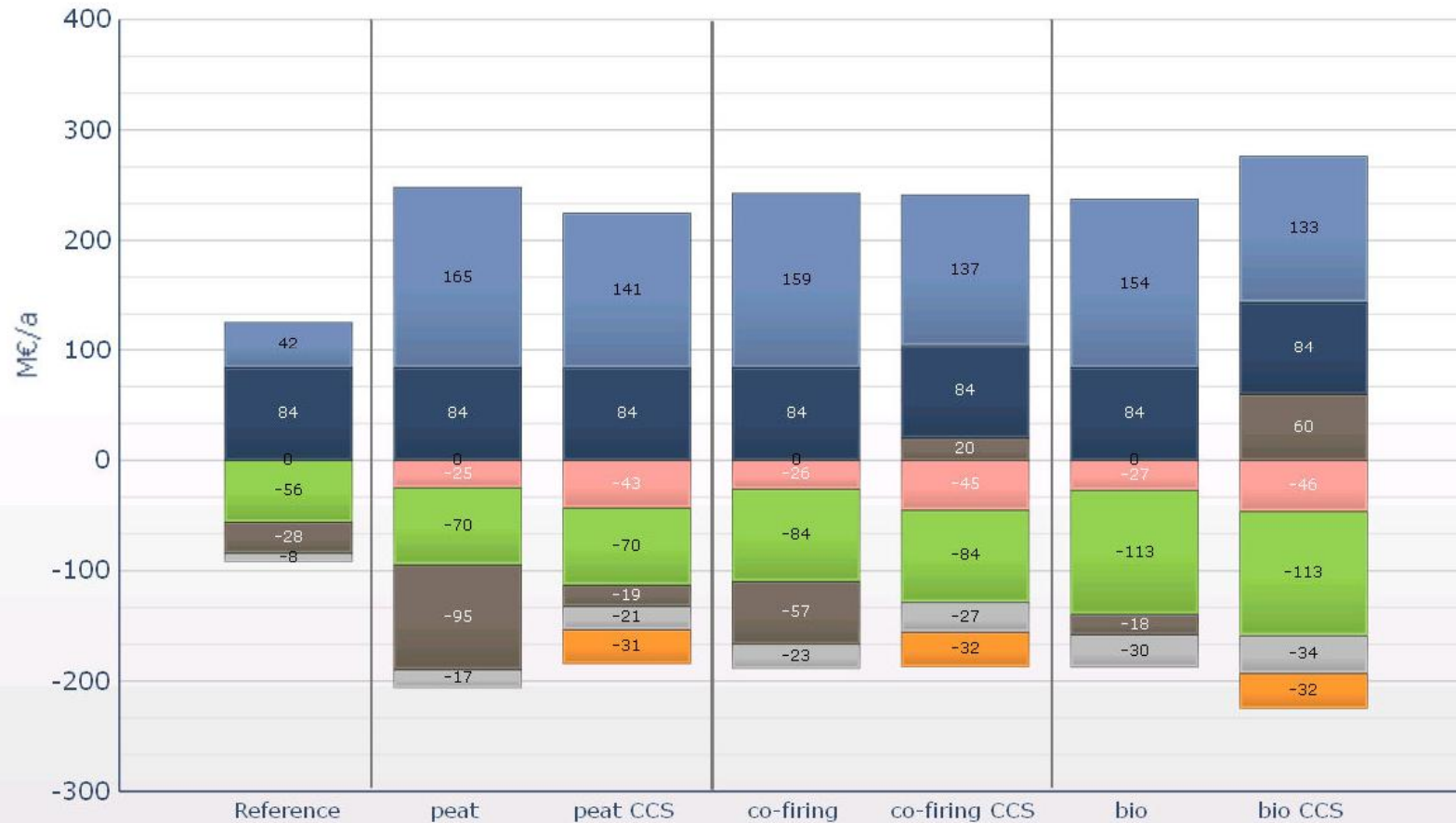
Profit and BeP

?

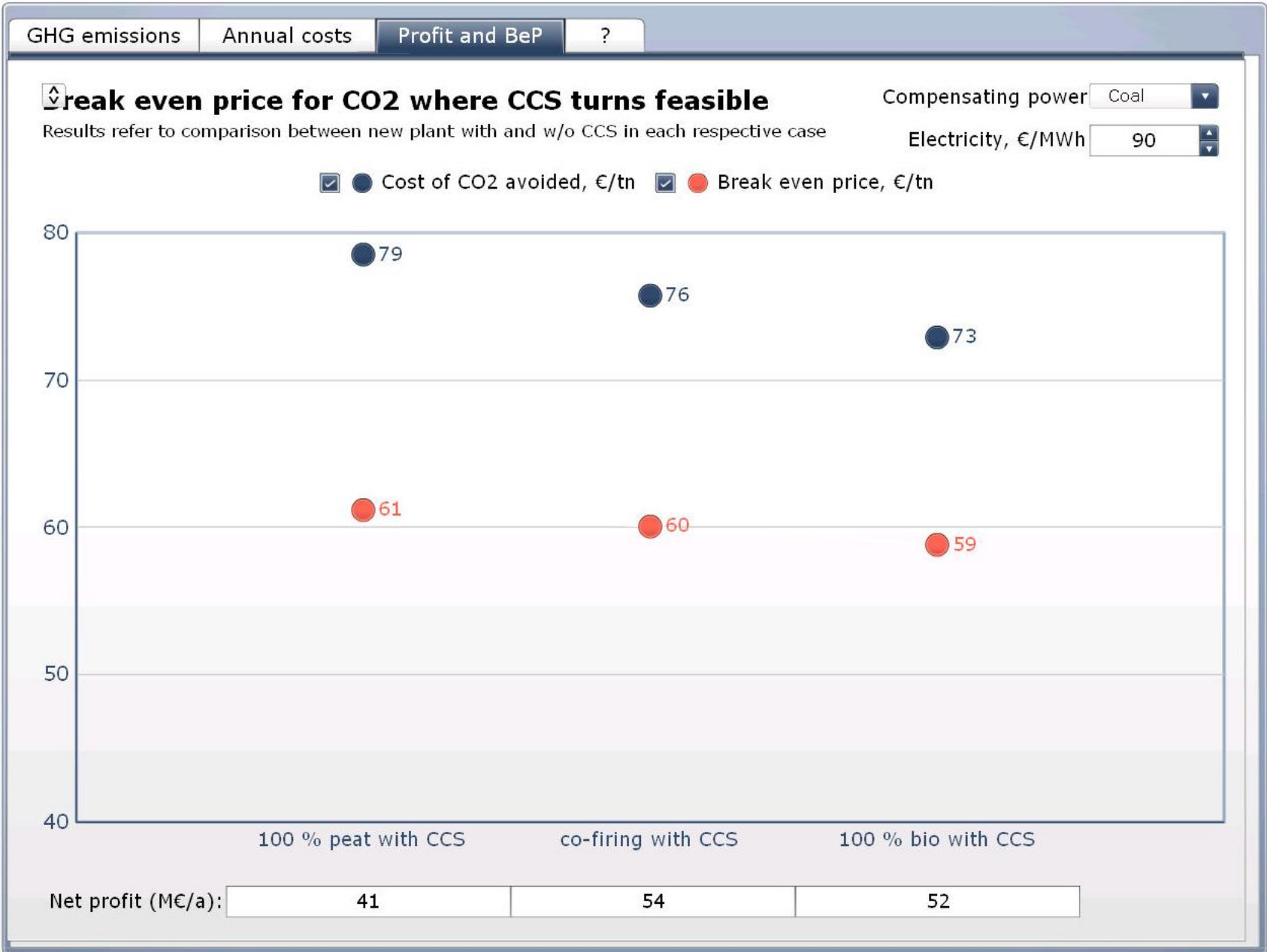
Annual operating costs and income, M€/a

Electricity, €/MWh 90
EU-ETS, €/tn 60

Capex
 Fuel
 CO2 ETS
 Other
 Transport and storage
 DH income
 Electricity income



Net profit:	34	42	41	54	54	50	52
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Conclusions on the case study

- The costs for CCS are heavily dependent not only on the characteristics of the facility and the operational environment but also on the chosen system boundaries and assumptions.
- In the case of Bio-CCS the investment and operational costs (excluding CO₂ emission allowances) are probably higher than in the case of fossil fuels. However, increasing CO₂ prices benefit Bio-CCS faster than other CCS options.
- Feasibility of Bio-CCS is strongly dependent on the CO₂ allowance price shift into biomass prices. In general, feasibility of CCS is dependent significantly on the CO₂ price shift into electricity price.
- The current EU ETS do not recognize negative emissions, and thus the economical incentive is not available for capturing CO₂ from biomass installations.



Thank you for your attention!

More information:

http://www.cleen.fi/en/program_overviews/ccsp_carbon_capture_and_storage_program

<http://www.vtt.fi/proj/ccsfinland/>

<http://www.vtt.fi/sites/flexiburncfb/>

